

Understanding the effects of multilayer assembly of tubular alumina-supported polyetherimide membranes on H₂, CO₂ and N₂ separation performance

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Abstract

Research in CO₂ capture and H₂ purification technology has garnered increased momentum due to global warming and world energy strategies. In this study, tubular polyetherimide (PEI) membranes were successfully prepared on the outer surface of tubular alumina (α -Al₂O₃) support using dip-coating and multilayer assembly techniques and examined for CO₂/N₂ and H₂/N₂ separations. This study systematically investigated the effects of support calcination temperature, polymer solution concentration, withdrawal speed, and the coating number of polymer layers on membrane gas separation performance in single and binary gas conditions.

The best PEI membrane prepared with substrate calcined at 1200 °C, 10 wt.% of PEI solution, 300 $\mu\text{m s}^{-1}$ of withdrawal speed, and three deposited layers produced gas permeances ($10^{-12} \text{ mol m}^{-2} \text{ s}^{-1} \text{ Pa}^{-1}$) of 310, 150 and 1 for H₂, CO₂ and N₂ respectively with a CO₂/N₂ and H₂/N₂ permselectivities of 149 and 308 (Figure 1).

In the binary gas testing, the membrane delivered an exclusive 100% permeate purity for CO₂ and H₂ in different feed gas concentrations and achieving maximum CO₂ and H₂ permeances of 4.3 and 6.0 $\times 10^{-10} \text{ mol m}^{-2} \text{ s}^{-1} \text{ Pa}^{-1}$, respectively. Suppression of glass transition temperature and crystallinity compared to the bulk polymer led to interfacial confinement phenomena which was confirmed by DSC, X-ray diffraction and Raman spectroscopic analyses [1]. The polymer interfacial confinement facilitated the exclusive H₂ and CO₂ transports without much affecting the N₂ permeance.

Keywords: Polyetherimide, Gas separation, CO₂ separation, multilayer assembly, Polymer confinement, Sintering temperature.

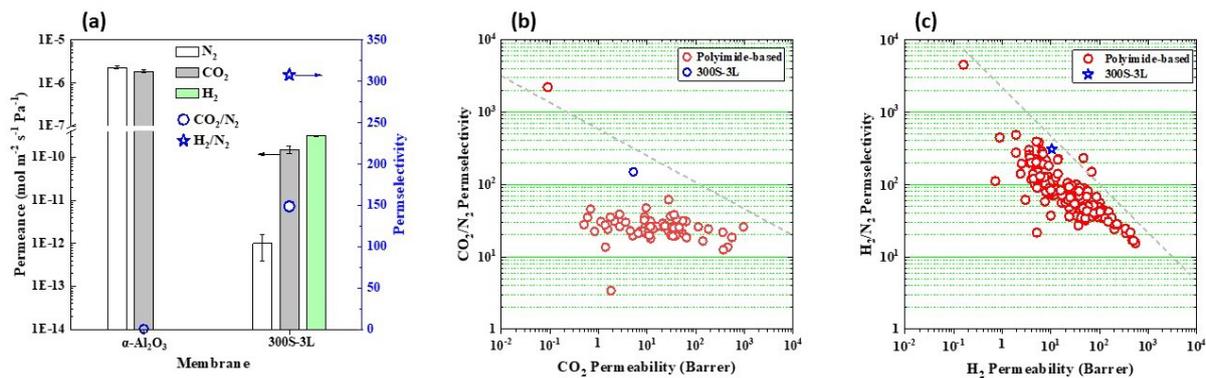


Figure 1. (a) Single gas permeance and selectivity of PEI/alumina membranes. A comparison plot for literature data of (a) CO₂/N₂, and (b) H₂/N₂ for polyimide-based membranes [2, 3]. The grey dash line represents 2008 Robson Upper bound.

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